Application No.: TBA (Based on PCT/EP03/007870) Docket No.: 12810-00012-US

AMENDMENTS TO THE CLAIMS

Claim 1 (currently amended): A process for increasing the yield in preparing polyhydric alcohols in increased yields comprising obtained by aldolizing formaldehyde with a higher aldehyde in the presence of catalytic amounts of a tertiary amine and hydrogenating the resulting mono- or polymethylolalkanals obtained in this way, especially of dimethylolbutanal to trimethylolpropane, which has the following steps, said process further comprising the steps of:

- a) distillative removal of the components having lower boiling points than the polyhydric alcohol from the crude product of the hydrogenation of the mono- or polymethylolalkanals;
- b) separation of the resulting bottom product in a second distillation stage into a high boiler fraction and a fraction comprising the majority of the polyhydric alcohol;
- c) acid treatment of the high boiler fraction, the water content of the high bolier fraction being from 20% to 90% by weight, based on the total amount of high boiler fraction and water; and
- d) distillation of the fraction comprising the majority of the polyhydric alcohol to remove the more volatile compounds (medium boiler fraction) and recovery of pure polyhydric alcohol;

wherein the acid-treated high boiler fraction is recycled into the hydrogenation of the mono- or polymethylolalkanes to the polyhydric alcohol.

Claim 2 (currently amended): <u>TheA</u> process <u>according to as claimed in claim 1</u>, wherein some or all of the medium boiler fraction removed from the fraction comprising the

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majority of the polyhydric alcohol by distillation is mixed with the high boiler fraction before the acid treatment.

Claim 3 (currently amended): <u>TheA</u> process <u>according to claim 1 as claimed in either of elaims 1 and 2</u>, wherein the acid concentration is from 0.1% by weight to 20% by weight, based on the total amount of high boiler fraction or the mixture of high boiler fraction and middle boiler fraction and water.

Claim 4 (currently amended): <u>TheA</u> process <u>according to claim 1 as claimed in any of elaims 1 to 3</u>, wherein the acid is selected from <u>the group consisting of C_1 - to C_{12} -carboxylic acids, C_2 - to C_{12} -dicarboxylic acids, sulfonic acids, mineral acids, carbon dioxide, sulfur dioxide and acidic ion exchangers.</u>

Claim 5 (currently amended): <u>TheA</u> process <u>according to claim 1 as claimed in any of claims 1 to 4</u>, wherein formic acid is used.

Claim 6 (currently amended): <u>TheA</u> process <u>according to claim 1 as claimed in any of elaims 1 to 5</u>, wherein the polyhydric alcohols are selected from the group <u>consisting</u> of trimethylolethane, trimethylolpropane, trimethylolbutane, neopentyl glycol and pentaerythritol.

Claim 7 (currently amended): <u>TheA</u> process <u>according to claim 1 as claimed in any of claims 1 to 6</u>, wherein the polyhydric alcohol is trimethylolpropane.

Claim 8 (new): The process according to claim 2, wherein the acid concentration is from 0.1% by weight to 20% by weight, based on the total amount of high boiler fraction or the mixture of high boiler fraction and middle boiler fraction and water.

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group consisting of C_1 - to C_{12} -carboxylic acids, C_2 - to C_{12} -dicarboxylic acids, sulfonic acids, mineral acids, carbon dioxide, sulfur dioxide and acidic ion exchangers.

Claim 10 (new): The process according to claim 3, wherein the acid is selected from the group consisting of C_1 - to C_{12} -carboxylic acids, C_2 - to C_{12} -dicarboxylic acids, sulfonic acids, mineral acids, carbon dioxide, sulfur dioxide and acidic ion exchangers.

Claim 11 (new): The process according to claim 8, wherein the acid is selected from the group consisting of C_1 - to C_{12} -carboxylic acids, C_2 - to C_{12} -dicarboxylic acids, sulfonic acids, mineral acids, carbon dioxide, sulfur dioxide and acidic ion exchangers.

Claim 12 (new): The process according to claim 2, wherein formic acid is used.

Claim 13 (new): The process according to claim 2, wherein the polyhydric alcohols are selected from the group consisting of trimethylolethane, trimethylolpropane, trimethylolbutane, neopentyl glycol and pentaerythritol.

Claim 14 (new): The process according to claim 3, wherein the polyhydric alcohols are selected from the group consisting of trimethylolethane, trimethylolpropane, trimethylolbutane, neopentyl glycol and pentaerythritol.

Claim 15 (new): The process according to claim 4, wherein the polyhydric alcohols are selected from the group consisting of trimethylolethane, trimethylolpropane, trimethylolbutane, neopentyl glycol and pentaerythritol.

Claim 16 (new): The process according to claim 5, wherein the polyhydric alcohols are selected from the group consisting of trimethylolethane, trimethylolpropane, trimethylolbutane, neopentyl glycol and pentaerythritol.

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Claim 17 (new): The process according to claim 2, wherein the polyhydric alcohol is trimethylolpropane.

Claim 18 (new): The process according to claim 3, wherein the polyhydric alcohol is trimethylolpropane.

Claim 19 (new): The process according to claim 4, wherein the polyhydric alcohol is trimethylolpropane.

Claim 20 (new): The process according to claim 5, wherein the polyhydric alcohol is trimethylolpropane.